

~~Grand Wang~~
#2 #1

The 2nd law of thermodynamics

5.79

same work:

2-3

4-1

addresses the direction of a process

heat flows from hot to cold
water flows downhill, etc.

Entropy is a measure of the
disorder in a system

Entropy is generated whenever

irreversibilities exist (friction,
directional processes).

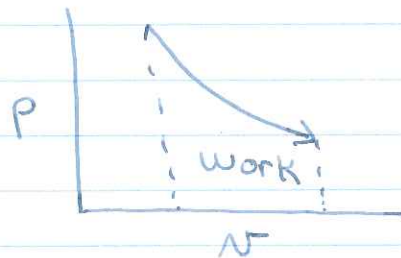
Entropy, S $\frac{\text{energy}}{\text{degree}}$ $\frac{\text{kJ}}{\text{K}}$

s $\frac{\text{energy}}{\text{mass deg}}$ $\frac{\text{kJ}}{\text{kg K}}$

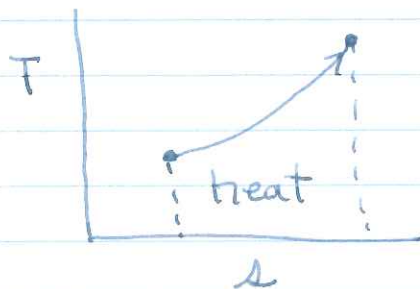
s evaluated like all other state
properties - use tables

$$s = \cancel{x s_f} + (1-x) s_f + x s_g$$

flow work
 $W = \int P dv$



$Q = \int T ds$



1st law

$$\Delta KE + \Delta PE + \Delta u = Q_{1-2} - W_{1-2}$$

frequently ϕ

$(dQ = du + dW)$ reversible sys.

$$dQ = T ds \quad dW = PdV$$

$$T ds = du + PdV$$

and/or

$$T ds = dH - VdP$$

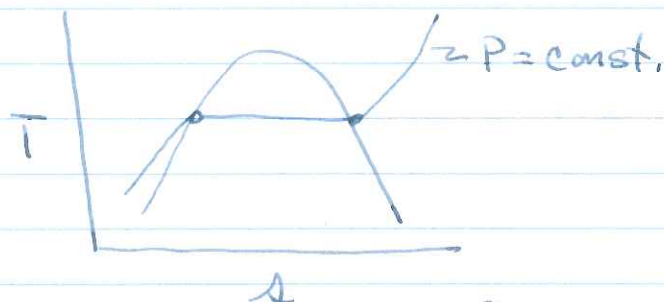
Recall $H = u + PV$ definition

$$dH = du + d(PV)$$

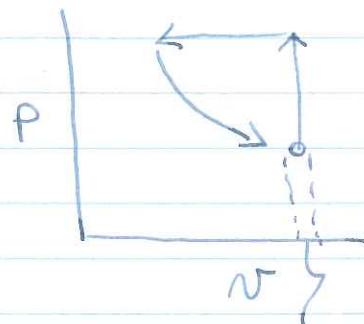
$$dH = du + PdV + VdP$$

$$dH - VdP = du + PdV$$

Take advantage of diagrams in analysis



$$Tds = dH - vdp$$



$$Tds = du + PdV$$

If in a liquid region (not wet)

~ incompressible i.e. $dv = 0$

$$Tds = du + PdV$$

$$\text{and } du = m du = m c_v dT$$

$$Tds = c_v dT$$

need to move like variables

$$ds = \frac{c_v dT}{T}$$

$$\int ds = \int \frac{c_v}{T} dT$$

$$s_2 - s_1 = c_v \ln(T_2/T_1) \text{ if } c_v \text{ constant (frequently)}$$

frequently an ideal gas assumption is reasonable.

$$T ds = du + P dv \quad ds = \frac{du}{T} + \frac{P}{T} dv$$

$$T ds = dh - v dP \quad ds = \frac{dh}{T} - \frac{v}{T} dP$$

$$du = c_v dT \quad dh = c_p dT$$

$$Pv = RT \quad \frac{P}{T} = \frac{R}{v} \Rightarrow ds = c_v \frac{dT}{T} + \frac{R}{v} dv$$

$$\frac{v}{T} = \frac{R}{P} \Rightarrow ds = c_p \frac{dT}{T} - \frac{R}{P} dP$$

integrating

$$s_2 - s_1 = \int \frac{c_v}{T} dT + R \ln(v_2/v_1)$$

$$s_2 - s_1 = \int \frac{c_p}{T} dT - R \ln(P_2/P_1)$$

Entropy balance for closed system

$$\text{Change in } S = \text{amt of } S \text{ transferred across bdy} + \text{amt of } S \text{ generated}$$

$$S_2 - S_1 = \int_1^2 \frac{dQ}{T} + \sigma$$

$$dQ > 0$$

$$S_2 > S_1$$

$\sigma > 0$
irreversibilities

$$dQ < 0$$

$$S_2 < S_1$$

(σ dependent)

$\sigma = 0$
reversible

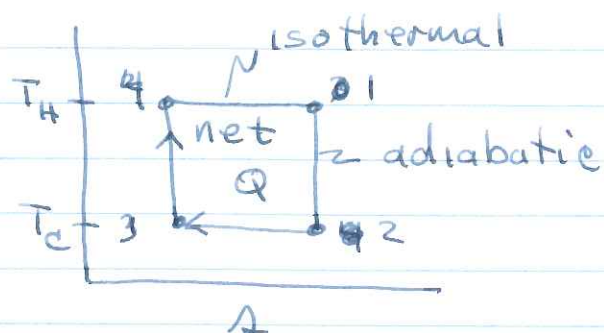
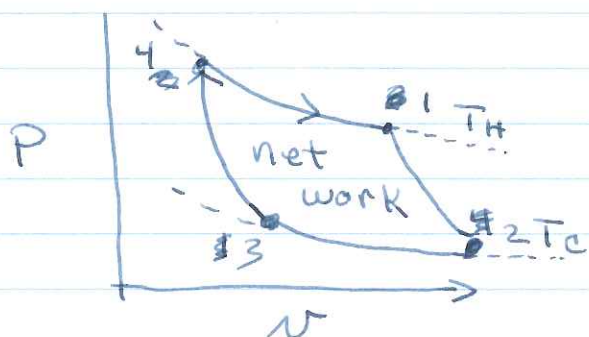
$\sigma < 0$
impossible

* a Carnot Cycle is defined as

4 reversible processes: two adiabatic processes alternated w/ two isothermal processes.

* Control Volume (open system)

$$\frac{dS}{dt} = \sum \frac{d\dot{Q}}{T} + \sum_{in} \dot{m} s - \sum_{out} \dot{m} s + \dot{\sigma}_{cv}$$



Process

~~1 → 2~~
3 → 4 : gas compressed adiabatically from T_C to T_H

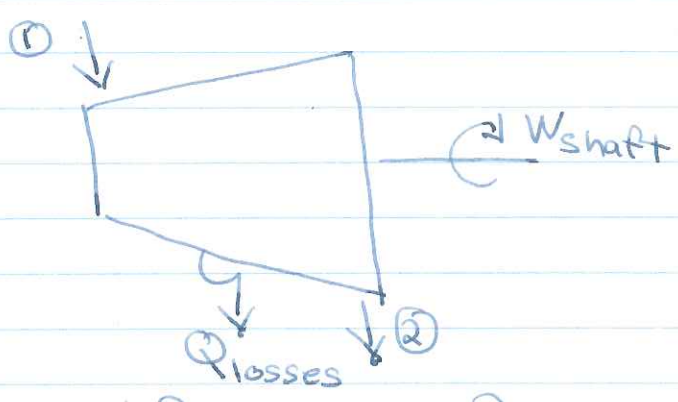
~~2 → 3~~
4 → 1 : gas expands isothermally receiving Q_H from reservoir at T_H

~~3 → 4~~
1 → 2 : gas expands adiabatically from T_H to T_C

~~4 → 1~~
2 → 3 : gas compresses isothermally to initial state releasing Q_C to reservoir at T_C

Consider:

Air enters a turbine



$$P_1 = 400 \text{ kPa}$$

$$T_1 = 970 \text{ K}$$

$$P_2 = 100 \text{ kPa}$$

$$T_2 = 670 \text{ K}$$

heat (Q) is lost from turbine surface
 at $T_{\text{sur, Avg}} = 315 \text{ K}$

$\dot{Q} \sim 30 \text{ kJ/kg}$ of air flowing

assume ideal gas $c_p = 1.01 \frac{\text{kJ}}{\text{kgK}}$

1st law $0 = \dot{Q} - \dot{W}_{cv} + \dot{m}(h_1 - h_2)$

$$\frac{\dot{W}_{cv}}{\dot{m}} = \frac{\dot{Q}_{cv}}{\dot{m}} + (h_1 - h_2) = \frac{\dot{Q}_{cv}}{\dot{m}} + c_p(T_1 - T_a)$$

$$\frac{\dot{W}_{cv}}{\dot{m}} = -30 \frac{\text{kJ}}{\text{kg}} + 1.01 \frac{\text{kJ}}{\text{kgK}} (970 - 670) = 300 \frac{\text{kJ}}{\text{kg}}$$

~~John Francis #10415~~

2nd law

$$0 = \frac{\dot{Q}_{cv}}{T} + \dot{m}(s_1 - s_2) + \dot{\sigma}_{cv}$$

$$\frac{\dot{\sigma}_{cv}}{\dot{m}} = -\frac{\dot{Q}_{cv}}{\dot{m}T} + (s_2 - s_1)$$

↓
Ideal gas const c_p

$$\frac{\dot{\sigma}_{cv}}{\dot{m}} = -\frac{\dot{Q}_{cv}/\dot{m}}{T_b} + c_p \ln\left(\frac{T_2}{T_1}\right) - R \ln P_2/P_1$$

$$R = 8.314 \frac{\text{kJ}}{\text{kmol K}} \frac{1}{28.97} \frac{\text{kmol}}{\text{kg}} = 0.287 \frac{\text{kJ}}{\text{kg K}}$$

$$\frac{\dot{\sigma}_{cv}}{\dot{m}} = -\frac{(-30 \text{ kJ/kg})}{315 \text{ K}} + \left[1.1 \ln\left(\frac{670}{970}\right) - 0.287 \ln\left(\frac{100}{400}\right) \right] \frac{\text{kJ}}{\text{kg K}}$$

$$= 0.086 \frac{\text{kJ}}{\text{kg K}} \quad \text{entropy generation}$$

if T_b smaller (i.e. bdy further away)
 $\dot{\sigma}$ larger (same \dot{Q} smaller T_b)